Statistical Optimization of Synthetic Soda Ash for Water Softening

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ABSTRACT
Synthesized soda ash was prepared by Solvay process with different molar ratio for application of water softening process. In urban utilization, water supply is very important for safe condition. In this research, Box-Behnken experimental design was employed for optimization of soda ash. The maximum yield percent of 19.882% of soda ash was obtained by the reaction salt to ammonium hydroxide to carbon dioxide (1:3:6.8) during the reaction time 90 min. The synthesized soda ash was analyzed by X-ray diffraction (XRD), Scanning Electron Microscope (SEM), Energy Dispersive X-ray Fluorescence (EDXRF) and Fourier Transform Infrared Spectroscopy (FTIR). Soda ash obtained from optimum condition was applied in water softening of tap water. According to the experimental results of water softening process, the maximum removal of hardness of water was observed at 3 ml of 10% lime solution with 20 ml of 5% of soda ash solution for 1000 ml of water. After treated the lime-soda process, the total hardness of water was reduced to initial condition of 255 ppm to 24 ppm.

KEYWORDS: Soda Ash, Optimization, Solvay, Water Softening, Total Hardness

I. INTRODUCTION
Soda ash also recognized as sodium carbonate is a white crystalline solid that is produced large amount in the world [1]. Commercial soda ash is highly purified and is sold in various grades that differ primarily in bulk density [2].

The objectives of water softening is to reduce the adverse effect of hard water. Hardness of water is caused by calcium and magnesium ions in water resulting from coming in contact with geological formations. The hardness interfere with the laundering of causing excess soap consumption, and may produce scales in small heaters and pipes. To a considerable extent these advantages have been overcome by the use of synthetic detergent and lining of pipes in small hot-water heaters. Industries generally preheat boiler water to prevent scaling [4].

For domestic uses, treated water must be aesthetically acceptable free from apparent turbidity, color, objectionable taste. Quality requirements for industrials uses frequently more stringent than domestic supplies [4].

II. MATERIALS AND METHODS
A. Raw Materials
The most important raw materials for preparation of soda ash are salt, ammonia, and carbon dioxide.
1. Salt: Salt is one of the most important raw materials in production of synthetic soda ash. It is inexpensive and easy to collect from local market. In its edible form of salt, it is commonly used in many industrial processes.
2. Ammonia Solution: Ammonia solution, also known as ammonium hydroxide, is a solution of ammonia in water. It can be denoted by the symbols NH₃ (aq). It is sometimes throughout of solution of ammonium hydroxide [5].

Nowadays, statistics plays an important role in research works and industrial applications. In this research work, Response Surface Methodology was used in consideration of experimental design. The response surface methodology RSM is a collection of mathematical and statistical techniques for empirical model building, design of experiments, and evaluating the effects of parameters [3]. In this research, soda ash was prepared by Box-Behnken experimental design to obtain optimum condition. The obtained soda ash was employed in water softening process.
this research, 25% of ammonia solution was used as raw material in soda ash preparation. It can be purchased from local market.

3. Carbon Dioxide: Carbon dioxide is a colorless gas with a density about 60% higher than that of dry air. Carbon dioxide consists of carbon atom covalently double bonded to one oxygen atoms \([6]\). In this research, it was used as a raw material in preparation of soda ash.

### B. Preparation of Raw Salt
Salt analysis was carried out to determine the specification of salt before purification. The raw salt composition was shown in Table I and analyzed by EDTA titration method \([7]\), Complex metric titration method \([8]\) and AOAC method \([9]\).

#### TABLE I. COMPOSITION OF RAW SALT SOLUTION

<table>
<thead>
<tr>
<th>Specification</th>
<th>ppm</th>
<th>Methods</th>
</tr>
</thead>
<tbody>
<tr>
<td>Total Hardness</td>
<td>448</td>
<td>EDTA Titration</td>
</tr>
<tr>
<td>Total Alkalinity</td>
<td>90</td>
<td>Complexometric Titration</td>
</tr>
<tr>
<td>Calcium</td>
<td>4</td>
<td>AOAC</td>
</tr>
<tr>
<td>Magnesium</td>
<td>23.04</td>
<td>AOAC</td>
</tr>
</tbody>
</table>

According to the analytical results, salt purification process was carried out by sedimentation process. The (300) gm of raw salt was mixed with (1000) ml of water. And then, it was stirred until the salt was completely dissolved. After that, it was settled to separate the clear solution and sediment. When the insoluble particles were settled, the clear solution was passed through the filter to remove the impurities. Finally, the filtrate was evaporated to 100 \(^{\circ}\)C, to obtain the clean salt.

### C. Preparation of Synthetic Soda Ash by Solvay process
The sodium chloride (25) gm was weighed and mixed with the 25% (w/w) of ammonia solution. And then; the mixture was stirred for a few minutes until all sodium chloride was completely dissolved. After that, when the carbon dioxide gas was passed through the solution and the reaction time was noted. The carbonation reaction was shown in equation 1\([10]\).

\[
\text{NaCl} + \text{NH}_4\text{OH} + \text{CO}_2 \rightarrow \text{NaHCO}_3 + \text{NH}_4\text{Cl} \quad (1)
\]

The reaction was proceeded until the significant amount of precipitates were started to form round about 1 hr. After 15 minutes, the precipitate of sodium bicarbonate was formed. And then, 15 minutes period was over, the reactor was put into the ice bath and cooled for 1 hr.

The cooled precipitated sodium bicarbonate was decanted into the conical flask by passing the clean funnel with whatman filter paper. And then precipitates were washed with cooled distilled water to remove unreacted salt and ammonium chloride. And then, it was calcined in muffle furnace at a temperature about 200\(^{\circ}\)C, carbon dioxide and water vapor was driven off. The calcinations reaction was shown in equation 2 \([10]\).

\[
2\text{NaHCO}_3 \rightarrow \text{Na}_2\text{CO}_3 + \text{H}_2\text{O} + \text{CO}_2 \quad (2)
\]

The calcined soda ash was ground with motor and pestle and finally soda ash was obtained.

According to this experimental procedure, the preliminary experiments were conducted at molar ratio of 1:1:1, 1:3:3 and 1:6:6 of salt to ammonium hydroxide to carbon dioxide gas. The experimental procedure for preparation of soda ash was shown in Figure 1.

![Figure 1. Preparation of Synthesized Soda Ash](image)

### III. RESULTS AND DISCUSSIONS
According to the preliminary experiments, the yield percent of soda ash was described in Table (II). Moreover, statistical designs were considered to provide the optimization of soda ash.

#### TABLE II. YIELD % OF SODA ASH FROM PRELIMINARY EXPERIMENTS

<table>
<thead>
<tr>
<th>Experiment No</th>
<th>Molar Ratio of NaCl: NH(_4)OH : CO(_2)</th>
<th>Reaction time(min)</th>
<th>Yield %</th>
</tr>
</thead>
<tbody>
<tr>
<td>1</td>
<td>1:1:1</td>
<td>90</td>
<td>9.72%</td>
</tr>
<tr>
<td>2</td>
<td>1:3:3</td>
<td>90</td>
<td>19.63%</td>
</tr>
<tr>
<td>3</td>
<td>1:6:6</td>
<td>90</td>
<td>16.9%</td>
</tr>
</tbody>
</table>

According to the yield percent of soda ash from preliminary experiments, independent variables and levels were considered and selected for design of experiment. The levels for each variable were shown in Table III. The experimental results were analyzed by ANOVA and the general equation which satisfied the statistical optimization was second order polynomial equation which was described as follow.

\[
Y = \beta_0 + \sum_{i=1}^{k} \beta_i x_i + \sum_{i=1}^{k} \beta_{ii} x_i^2 + \sum_{i=1}^{k} \sum_{j=i+1}^{k} \beta_{ij} x_i x_j + \varepsilon \quad (3)
\]
Where, Y is the predicated response of the yield % of soda ash, xi, xj are the independent variables, $\beta_0$, $\beta_1$, $\beta_2$, $\beta_3$ are the regression coefficient of intercept, linear, quadratic and interaction effects respectively and $\epsilon$ is the random error [3].

The experimental runs generated with yield percent of soda ash were shown in table (IV). The analysis of variance for the experimental results was shown in table (V).

### TABLE III INDEPENDENT VARIABLES AND LEVELS FOR BOX-BEHNKEN DESIGN

<table>
<thead>
<tr>
<th>Variables</th>
<th>Symbols</th>
<th>Level (-1)</th>
<th>Level (0)</th>
<th>Level (1)</th>
</tr>
</thead>
<tbody>
<tr>
<td>Ammonium Hydroxide (mol)</td>
<td>X₁</td>
<td>3</td>
<td>4.5</td>
<td>6</td>
</tr>
<tr>
<td>Carbon Dioxide (mol)</td>
<td>X₂</td>
<td>3</td>
<td>7.5</td>
<td>12</td>
</tr>
<tr>
<td>Reaction Time (min)</td>
<td>X₃</td>
<td>90</td>
<td>135</td>
<td>180</td>
</tr>
</tbody>
</table>

### TABLE IV BOX-BEHNKEN DESIGN MATRIX, EXPERIMENTAL YIELD % AND PREDICTED YIELD % OF SODA ASH

<table>
<thead>
<tr>
<th>No</th>
<th>Run No</th>
<th>X₁</th>
<th>X₂</th>
<th>X₃</th>
<th>Experimental Yield %</th>
<th>Predicted Yield %</th>
</tr>
</thead>
<tbody>
<tr>
<td>1</td>
<td>1</td>
<td>-1</td>
<td>0</td>
<td>1</td>
<td>9.60</td>
<td>9.42</td>
</tr>
<tr>
<td>2</td>
<td>2</td>
<td>0</td>
<td>-1</td>
<td>1</td>
<td>6.60</td>
<td>6.47</td>
</tr>
<tr>
<td>3</td>
<td>3</td>
<td>0</td>
<td>1</td>
<td>-1</td>
<td>1.70</td>
<td>1.83</td>
</tr>
<tr>
<td>4</td>
<td>4</td>
<td>-1</td>
<td>0</td>
<td>-1</td>
<td>22.12</td>
<td>19.88</td>
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<td>5</td>
<td>5</td>
<td>1</td>
<td>0</td>
<td>1</td>
<td>15.68</td>
<td>17.92</td>
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<tr>
<td>6</td>
<td>6</td>
<td>-1</td>
<td>1</td>
<td>0</td>
<td>0.36</td>
<td>2.46</td>
</tr>
<tr>
<td>7</td>
<td>7</td>
<td>1</td>
<td>1</td>
<td>0</td>
<td>0.20</td>
<td>-0.10</td>
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<tr>
<td>8</td>
<td>8</td>
<td>-1</td>
<td>-1</td>
<td>0</td>
<td>6.62</td>
<td>6.50</td>
</tr>
<tr>
<td>9</td>
<td>9</td>
<td>0</td>
<td>0</td>
<td>0</td>
<td>4.34</td>
<td>4.34</td>
</tr>
<tr>
<td>10</td>
<td>10</td>
<td>1</td>
<td>-1</td>
<td>0</td>
<td>0.12</td>
<td>-1.98</td>
</tr>
<tr>
<td>11</td>
<td>11</td>
<td>1</td>
<td>0</td>
<td>-1</td>
<td>0.16</td>
<td>0.33</td>
</tr>
<tr>
<td>12</td>
<td>12</td>
<td>0</td>
<td>0</td>
<td>0</td>
<td>4.04</td>
<td>4.34</td>
</tr>
<tr>
<td>13</td>
<td>13</td>
<td>0</td>
<td>0</td>
<td>0</td>
<td>4.64</td>
<td>4.34</td>
</tr>
<tr>
<td>14</td>
<td>14</td>
<td>0</td>
<td>1</td>
<td>1</td>
<td>6.40</td>
<td>4.46</td>
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<tr>
<td>15</td>
<td>15</td>
<td>0</td>
<td>-1</td>
<td>-1</td>
<td>0.04</td>
<td>1.97</td>
</tr>
</tbody>
</table>

### TABLE V. ANALYSIS OF VARIANCE FOR YIELD % OF SODA ASH

<table>
<thead>
<tr>
<th>Source</th>
<th>Df</th>
<th>SS</th>
<th>Adj MS</th>
<th>F value</th>
<th>P value</th>
<th>R²</th>
<th>R² adj</th>
</tr>
</thead>
<tbody>
<tr>
<td>Regression</td>
<td>9</td>
<td>532.768</td>
<td>59.196</td>
<td>11.03</td>
<td>0.008</td>
<td>95.20%</td>
<td>86.57%</td>
</tr>
<tr>
<td>linear</td>
<td>3</td>
<td>88.892</td>
<td>29.631</td>
<td>5.52</td>
<td>0.048</td>
<td></td>
<td></td>
</tr>
<tr>
<td>Square</td>
<td>3</td>
<td>237.690</td>
<td>79.230</td>
<td>14.76</td>
<td>0.006</td>
<td></td>
<td></td>
</tr>
<tr>
<td>Interaction</td>
<td>3</td>
<td>206.187</td>
<td>68.729</td>
<td>12.80</td>
<td>0.009</td>
<td></td>
<td></td>
</tr>
<tr>
<td>Error</td>
<td>5</td>
<td>26.841</td>
<td>5.368</td>
<td></td>
<td></td>
<td></td>
<td></td>
</tr>
<tr>
<td>Lack of fit</td>
<td>3</td>
<td>26.661</td>
<td>8.887</td>
<td>98.74</td>
<td>0.01</td>
<td></td>
<td></td>
</tr>
<tr>
<td>Pure Error</td>
<td>2</td>
<td>0.180</td>
<td>0.090</td>
<td></td>
<td></td>
<td></td>
<td></td>
</tr>
</tbody>
</table>

Yield % = 129.3 - 28.68 X₁ + 3.21 X₂ - 62.7 X₃ + 1.241 X₁² - 0.2673 X₂² + 8.46 X₃² + 0.219 X₁X₂ + 6.23 X₁X₃ - 0.138 X₂X₃ (4)

F-value and P-value were used to check the significance of the model. According to the ANOVA table , the P-value of the model was less than 0.05, which described that it was a significant model. Based on 95 % confidence level , the model was confirmed to be significant as the computed F value , (11.03) was much higher than that the theoretical F value $F_{0.05(9,5)} (4.77)$. The high value of $R^2$ and $R^2 _{adj}$ representing the high degree of correlation between the experimental yield % and predicted yield %. The coefficient of determinations ($R^2$) was 95.20% which indicated that the model was significantly effected and represented the real relationship among the parameters. So ,it can be said a fitted model [11].

The optimum value of 19.882 % was obtained at molar ratio of salt to ammonium hydroxide to carbon dioxide 1:3: 6.8 and reaction time 1.50 hr. When this optimization was validated with the experiment, it gave percent conversion of yield percent of 19 %. It can be found that error percent of 4.4 which was acceptable within the range of 95 % confidence level.

### D. Characterizations of Soda Ash

The products were analyzed by X-ray diffraction (XRD), Scanning Electron Microscopy (SEM), Energy Dispersive X-rays Fluorescence (EDXRФ), and Fourier Transform-Infrared Spectroscopy (FTIR).

#### 1. X-ray diffraction (XRD)

The XRD patterns of soda ash from experiment 1, experiment 2, experiment 3 and optimum condition of soda ash from Box- Behnken experimental design was shown in Figure. 2 . They were compared to standard soda ash. According to the XRD patterns, experiment 1, experiment 2 and experiment 3 have thirteen characteristic peaks. However the soda ash which prepared by optimum condition of Box-Behnken experimental design was more clear and favorable. It has thirteen characteristics peaks and observed at angle 2θ (27.188), (29.953), (34.021), (33.082), (34.354), (35.055), (37.736), (39.705), (41.215), (41.460), (53.423), (56.874), (62.419) were corresponding to (201), (002), (020), (-202), (-112), (310), (112), (202), (200), (-
were aggregated and some were scattered. shapes of soda ash samples were ge experiment 2 and 3. According to the SEM images , the image of soda ash from optimum condition was shown in experiment 3 was cylindrical shape. The morphology of experiment 1 and experiment 2 were rod shape and they were aggregated to each other. The SEM image from experiment 3 was cylindrical shape. The morphology of SEM image of soda ash from optimum condition was shown in Fig.6. It was more aggregate and fine than experiment 1, experiment 2 and 3. According to the SEM images, the shapes of soda ash samples were generally in rod shape and they were formed as crystalline structure. Some of them were aggregated and some were scattered.

2. **Scanning Electron Microscopy (SEM)**
In this study, the morphology of synthetic soda ash were determined by Scanning Electron Microscopy (SEM). The SEM images of soda ash from experiment 1, 2 and 3 were shown in Fig. 3,4 and 5. According to the SEM images, experiment 1 and experiment 2 were rod shape and they were aggregated to each other. The SEM image from experiment 3 was cylindrical shape. The morphology of SEM image of soda ash from optimum condition was shown in Fig.6. It was more aggregate and fine than experiment 1, experiment 2 and 3. According to the SEM images, the shapes of soda ash samples were generally in rod shape and they were formed as crystalline structure. Some of them were aggregated and some were scattered.

3. **Energy Dispersive X-ray Fluorescence (EDXRF)**
Quantitative results of soda ash were analyzed by using Energy Dispersive X-rays Fluorescence (EDXRF). According to the EDXRF results, carbon percent from experiment (1), experiment (2) and experiment (3) were 7.07%, 6.08% and 7.27% respectively. Sodium percent from experiment (1), experiment (2) and experiment (3) were 92.64%, 93.73% and 92.53% respectively. According to the experimental results, the optimum condition of soda ash was analyzed by Fourier Transform Infread Spectroscopy (FTIR).

4. **Fourier Transform Infrared Spectroscopy (FTIR)**
The optimum condition of soda ash prepared by Box-Behnken experimental design was analyzed by Fourier Transform Infrared Spectroscopy. The spectra was recorded in the range (500-4000 cm\(^{-1}\)). According to the infrared spectrum of soda ash, the stretching bonds of (O-H) were observed at approximately 3500 cm\(^{-1}\) and 3000 cm\(^{-1}\) respectively and have been attributed to hydroxyl group. The stretching bond of (C-O) was occurred at 1454.38 cm\(^{-1}\). The stretching bond of (C-CL) was occurred at 858.38 cm\(^{-1}\). The stretching bond of (C-CL) was occurred at 858.38 cm\(^{-1}\) that is due to the impurities in the sample. The infrared spectrum of soda ash from optimum condition is nearly the same as the standard soda ash [11].

![Figure. 2. XRD patterns of Synthetic Soda Ash](image)

![Figure. 3. SEM image of Soda Ash from Experiment 1](image)

![Figure. 4. SEM image of Soda Ash from Experiment 2](image)

![Figure. 5. SEM image of Soda Ash from Experiment 3](image)

![Figure. 6. SEM image of Soda Ash from Optimum Condition](image)

![Figure. 7. Infrared Spectrum of Standard Soda Ash](image)
E. Application of Soda Ash

According to the analytical results of the synthetic soda ash, it was confirmed as soda ash. It was applied in water softening process for removal of total hardness of water. Water sample was taken from the laboratory of Chemical Engineering Department from West Yangon Technological University Campus, Hlaing Tharyar Township, Yangon Region. Water analysis was carried out by APHA standard methods. The characterization of raw water was shown in Table (VI).

**TABLE (VI). Characterization of Raw Water**

<table>
<thead>
<tr>
<th>No</th>
<th>Specifications</th>
<th>Value</th>
</tr>
</thead>
<tbody>
<tr>
<td>1</td>
<td>Total Hardness(ppm)</td>
<td>255</td>
</tr>
<tr>
<td>2</td>
<td>Total Alkalinity(ppm)</td>
<td>85</td>
</tr>
<tr>
<td>3</td>
<td>Calcium(ppm)</td>
<td>47</td>
</tr>
<tr>
<td>4</td>
<td>Magnesium(ppm)</td>
<td>4.37</td>
</tr>
<tr>
<td>5</td>
<td>Sulfate(ppm)</td>
<td>43.1</td>
</tr>
<tr>
<td>6</td>
<td>Chloride(ppm)</td>
<td>400</td>
</tr>
<tr>
<td>7</td>
<td>Iron(ppm)</td>
<td>28</td>
</tr>
<tr>
<td>8</td>
<td>pH</td>
<td>7.9</td>
</tr>
</tbody>
</table>

F. Water Softening

1. Precipitatives Softening

Precipitatives softening uses lime (Ca(OH)$_2$) and soda ash (Na$_2$CO$_3$) to remove calcium and magnesium ions from solution. Lime added to water reacts first with free carbon dioxide forming a calcium carbonate precipitate. The lime reacts with free carbon dioxide forming a calcium bicarbonate present. In both of these equation one equivalent of lime reacts with free carbon dioxide forming a calcium carbonate precipitate. The lime reacts with any calcium bicarbonate present. In both of these equations, one equivalent of lime combines with one equivalent of either CO$_2$ or Ca(HCO$_3$)$_2$.

\[
\text{CO}_2 + \text{Ca(OH)}_2 \rightarrow \text{CaCO}_3 \uparrow + \text{H}_2\text{O} \quad [4]
\]

\[
\text{Ca(HCO}_3\text{)}_2 + \text{Ca(OH)}_2 \rightarrow 2\text{CaCO}_3 \uparrow + 2\text{H}_2\text{O} \quad [5]
\]

Since magnesium precipitates as Mg(OH)$_2$

\[
\text{Mg} (\text{HCO}_3\text{)}_2 + \text{Ca(OH)}_2 \rightarrow \text{MgCO}_3 \downarrow + \text{CaCO}_3 \uparrow + 2\text{H}_2\text{O} \quad [6]
\]

\[
\text{MgCO}_3 + \text{Ca(OH)}_2 \rightarrow \text{Mg(OH)}_2 \downarrow + \text{CaCO}_3 \uparrow \quad [7]
\]

Removal of Carbonate hardness with lime

\[
\text{Ca}^{2+} + 2\text{HCO}_3^- + \text{Ca(OH)}_2 \rightarrow 2\text{CaCO}_3 \downarrow + 2\text{H}_2\text{O} \quad [9]
\]

\[
\text{Ca}^{2+} + \text{SO}_4^{2-} + \text{Na}_2\text{CO}_3 \rightarrow \text{CaCO}_3 \downarrow + 2\text{Na}^+ + 2\text{Cl}^- \quad [11]
\]

Removal of non-carbonate hardness with soda ash and lime

\[
\text{Ca}^{2+} + 2\text{Cl}^- + \text{Na}_2\text{CO}_3 \rightarrow \text{CaCO}_3 \downarrow + 2\text{Na}^+ + 2\text{Cl}^- \quad [12]
\]

\[
\text{Mg}^{2+} + 2\text{CO}_3^{2-} + 2\text{Ca(OH)}_2 \rightarrow 2\text{Mg(OH)}_2 \downarrow + 2\text{CaCO}_3 \downarrow + 2\text{H}_2\text{O} \quad [13]
\]

Recarbonation for pH Control

\[
\text{CO}_3^{2-} + \text{CO}_2 + \text{H}_2\text{O} \rightarrow 2\text{HCO}_3^- \quad [15]
\]

In this research, water softening process was carried out by various dosage of lime and soda ash. Experiment (I) was carried out by single-stage lime-softening process. Experiment (II) was carried out by synthesized soda ash. Experiment (III) was carried out by water softening by using both lime and synthesized soda ash. Experiment (IV) was carried out by water softening by using both lime and commercial soda ash.

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According to this graph, when lime dosage was increased, pH was steadily increased. However, lime dosage was exceeded over the required level, hardness of water was returned to increase. According to this graph, only lime solution can not reduced the total hardness significantly.

2. Procedure of Water Softening Process With Synthesized Soda Ash

In experiment (II), raw water (100) ml was taken to treat with 5% synthesized soda ash solution. And then it was stirred by magnetic stirrer with 500 rpm. After that, it was settled for 10 min and passed through a filter paper. The soda ash treated water was analyzed by EDTA titration method to know the removal efficiency of total hardness.

According to the experimental results, hardness of water was affected by various dosage of soda ash. When the dosage was increased, the pH of water was significantly increased. So, the hardness and pH of water were inversely proportional according to the dosage of soda ash. However, the dosage of synthesized soda ash was exceeded over the required level, hardness level of water was increased significantly. The effect of synthesized soda ash vs total hardness and pH was shown in Figure 9.

![Figure 9. Effect of Total Hardness and pH with Various Dosage of Synthesized Soda Ash Solution](image)

According to this graph, pH level was sharply raised when the dosage was increased. The hardness of water was significantly decreased from initial condition of 255 ppm to 171 ppm. However, hardness level was returned to increase when the dosage was increased.

3. Procedure of Water Softening Using Both Lime and Synthesized Soda Ash

In experiment (III), water sample was treated by using both lime and synthesized soda ash. According to the lime process, 0.3 ml of lime was taken as optimum condition because which removed the hardness than other dosage. According to the lime dosage, the pH level of water was raised; the bicarbonates ions were converted to carbonate concentration. Due to the increase in carbonate concentration, precipitates of calcium carbonate were formed. The remaining calcium cannot be removed by simple adjustment of pH. So, soda ash solution was added by varying the dosage to precipitates the remaining calcium. In lime-soda treatment, the pH level was raised by addition of lime while sodium carbonate was added to reduce residual carbonate hardness. The treated water was passed through the filter paper, and then it was analyzed by EDTA titration method.

According to the experiment, lime and various dosage of synthesized soda ash was effectively reduced the water hardness. Maximum removal percent of hardness of water was observed at 0.3 ml of lime and 2 ml of synthesized soda ash. The effect of both lime and soda ash dosage vs pH and total hardness was shown in Fig. 10.

![Figure 10. Effect of Lime-Soda Dosage by Synthesized Soda Ash](image)

According to this graph, hardness of water was dramatically decreased but pH of water was increased. When the dosage of was increased over the required level, the hardness level of water was slightly increased.


In experiment IV, lime-soda softening process was carried out using the commercial grade soda ash to reduce the hardness of water. The procedure was the same as using the lime and various synthesized soda ash.

According to the results, water softening by using both lime and commercial soda ash dosage effectively reduced the water hardness. The maximum removal of hardness of water was observed at 0.3 ml of lime and 2 ml of commercial soda ash. The effect of lime and soda ash dosage on pH and total hardness was shown in Figure 11.

![Figure 11. Effect of lime and various dosage of commercial soda ash](image)

According to this graph, hardness of water was dramatically decreased but pH of water was increased. When the dosage was increased over the required level, the hardness level of water was slightly increased.
5. **Jar Testing**

Firstly, one liter of sample water was taken and added to each of the beakers of gang-mixer system. The mixers in each beaker were allowed to set a mixing rate of 150 rpm. Next, 5% of commercial grade sodium carbonate solution was added into the first beaker. And then, 5% of synthesized soda ash solution was added into the second beaker and allowed to mix with 150 rpm. According to the lime-soda softening process, the optimum condition of 3 ml of lime solution was added into the third and fourth beakers. After 10 minutes, the beakers were allowed to settle. Following the settling period, the samples were collected from each beaker and filtered. The pH levels were measured for adjusting the optimum range.

After that, 5% synthesized soda ash solution was added into lime treated water by varying dosage. The mixers in each beaker were allowed to set up the 150 rpm. After 10 minutes, the beakers were allowed to settle for 10 minutes. After settling, the samples were filtered. The pH was measured before and after filtration. And then it was passed through by carbon dioxide gas to obtain the acceptable pH range of (6.5 - 8.5). Finally, the treated waters were measured pH and total hardness.

According to the jar testing results, lime-soda softening process was more effectively reduced the hardness of water than only synthesized soda ash dosage. Water softening by using both synthesized soda ash dosage and lime is more effective. According to the lime-soda softening process, the optimum condition for one liter water was observed at 3 ml of lime and 20 ml of synthesized soda ash. And then, the treated water from the optimum condition was passed through by carbon dioxide to obtain acceptable pH range of 6.5 ~ 8.5. Finally, it was measured to total hardness, total alkalinity, calcium, magnesium, sulfate, chloride and iron. The result of treated water by jar test was shown in Table VII. The Specifications of treated water was shown in Table VIII.

<table>
<thead>
<tr>
<th>Run No</th>
<th>Volume of Sample Water (ml)</th>
<th>10% lime Solution</th>
<th>5%Soda Ash Solution (ml)</th>
<th>Settling Tim(min)</th>
<th>pH</th>
<th>Total Hardness</th>
<th>Hardness Removal %</th>
</tr>
</thead>
<tbody>
<tr>
<td>1</td>
<td>1000</td>
<td>-</td>
<td>20</td>
<td>10</td>
<td>9</td>
<td>185</td>
<td>27.45</td>
</tr>
<tr>
<td>2</td>
<td>1000</td>
<td>-</td>
<td>-</td>
<td>20</td>
<td>10</td>
<td>175</td>
<td>31.72</td>
</tr>
<tr>
<td>3</td>
<td>1000</td>
<td>3</td>
<td>20</td>
<td>10</td>
<td>9.5</td>
<td>24</td>
<td>90.59</td>
</tr>
<tr>
<td>4</td>
<td>1000</td>
<td>3</td>
<td>10</td>
<td>10</td>
<td>9</td>
<td>26</td>
<td>89.80</td>
</tr>
</tbody>
</table>

**Table VIII Specification of Treated Water**

<table>
<thead>
<tr>
<th>No</th>
<th>Specifications</th>
<th>Raw Water Value</th>
<th>Treated Water Value</th>
</tr>
</thead>
<tbody>
<tr>
<td>1</td>
<td>Total Hardness (ppm)</td>
<td>255</td>
<td>24</td>
</tr>
<tr>
<td>2</td>
<td>Total Alkalinity (ppm)</td>
<td>85</td>
<td>240</td>
</tr>
<tr>
<td>3</td>
<td>Calcium (ppm)</td>
<td>47</td>
<td>9.02</td>
</tr>
<tr>
<td>4</td>
<td>Magnesium (ppm)</td>
<td>4.37</td>
<td>0.2</td>
</tr>
<tr>
<td>5</td>
<td>Sulfate (ppm)</td>
<td>43.1</td>
<td>45.2</td>
</tr>
<tr>
<td>6</td>
<td>Chloride (ppm)</td>
<td>400</td>
<td>370</td>
</tr>
<tr>
<td>7</td>
<td>Iron (ppm)</td>
<td>28</td>
<td>&lt;</td>
</tr>
<tr>
<td>8</td>
<td>pH</td>
<td>7.9</td>
<td>6.5</td>
</tr>
</tbody>
</table>

According to the experimental results, the concentration of raw water and the treated water were different. Lime-soda softening process was reduced the hardness from initial concentration of 255 ppm to 24 ppm. However, the total alkalinity was increased from initial condition of 85 ppm to 240 ppm according to the lime dosage. Calcium, magnesium and iron were dramatically reduced from initial concentrations because of lime and soda ash dosage. Sulfate was slightly increased from initial concentration of 43.1 to 45.2 ppm. Chloride was slightly reduced from 400 ppm to 370 according to lime-soda dosage. Before carbonation, pH of treated water is 9.5; it was reduced to pH 6.5 by passing carbon dioxide gas. It was within the acceptable level. The initial pH of raw water is 7.9. The final pH of treated water was 6.5.

### IV. CONCLUSIONS

In this study, the soda ash is prepared synthetically by Solvay process by the use of Box-Behnken experimental design. The maximum yield percent of 19.882% was obtained with the reaction salt to ammonium hydroxide to carbon dioxide ratio of 1:3:6.8 during reaction time 90 minutes. According to the XRD patterns, SEM images and FTIR result, the optimum condition which prepared by Box-Behnken experimental design is said to soda ash and applied in water softening process.

Water softening was carried out by lime softening, softening by synthesized soda ash, softening by commercial soda ash and lime-soda softening process. According to the experimental results, lime softening process cannot adequately reduce the hardness level. Softening by synthesized and commercial soda ash can reduce the hardness level of water.

However, the lime-soda process can effectively reduce the hardness level of water. The initial characteristics of raw water is total hardness of 255 ppm, total alkalinity of 85 ppm, calcium of 47 ppm, magnesium of 4.37 ppm, sulfate of 43.1 ppm, chloride of 400 ppm, iron of 28 ppm. The initial pH is 7.9. After lime-soda treatment, the total hardness of 24, total alkalinity of 240, Calcium of 9.02, Magnesium of 0.2, Sulfate of 45.2%, Chloride of 270, Iron of < 0.1 and pH of 6.5 are obtained.
ACKNOWLEDGEMENT
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REFERENCES